

Guideline on the safety related requirements of the ChemCar-Competition Rev. 12

ChemCar 2024

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Introduction

This guideline lists question complexes, documentations and verifications that are required for the safety consideration of the submitted ChemCar Safety Concepts. Without these documents and verifications, a qualified evaluation of the concepts is not possible and thus a security approval cannot be issued.

For clarification, an example of the documentation of the technical data of a ChemCar team in recent years is set at the end of this guideline. This example includes the calculations for estimating the developing reaction heat and the maximum pressure expected (see chapters 7 - 9). Please note that this example provides information only on the form and on the detail of the document but not on the content.

General Notes for making the safety concept:

- For preparation of the safety concept (including a risk assessment) it is necessary to answer the questions and remind the hints given at points 1. 6. of this document. It is a <u>non-exhaustive</u> <u>enumeration</u>, what means hazards resulting from your ChemCar in special must be assessed and discussed by yourself.
- The safety concept that includes the risk assessment has to be done as an independent document (additional to the concept templates of kjVI).

1. Pressure

- Pressure units:
 - Use consistent pressure units absolute pressure [bar_{abs}] or relative pressure [bar_g]
- Operating pressure:
 - What is the pressure in normal operation of the ChemCar?

It is always necessary to document a pressure and give a description why this pressure defines normal operation.

- Maximum pressure expected:
 - What is the maximum pressure reached by reaction if pressure vessel is blocked by malfunction?

A worst-case scenario must be considered. Please discuss what assumptions were made for worst-case.

- Pressure test / manufacturer certificate:
 - Attach the results of the pressure tests performed or hand in a manufacturer certificate.
 When using a pressure system, a pressure test for the overall system might be necessary even if a manufacturer certificate is available. The requirements and the performance of the pressure test are specified in the ChemCar Safety Rules.

If pressure test, manufacturer certificate or both are not necessary for operation of the ChemCar, please give a comprehensible explanation.

- Safety valve:
 - All the calculations for the design of the used safety valve (e.g., according to AD-Merkblatt
 Must be provided comprehensibly. Not only the results!

If a safety valve is not necessary for safe operation, please give a comprehensible explanation.

- Pressure gauge / indicator
 - Ensure that the ChemCar has a suitable pressure gauge / indicator, which has to be included in the process flowchart. It must be possible to read the internal pressure of the ChemCar at any condition (e. g. in case of breakdown of ChemCar)

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If a pressure gauge / indicator is not necessary for safe
operation, please give a comprehensible explanation.
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In accordance with the ChemCar Safety Rules you should pay attention that the pressure content product (pressure * volume) does not exceed 50 [bar * L] as far as possible (scope of pressure equipment directive 2014/68/EU; directive 2009/104/EC "minimum health and safety requirements for the use of work equipment by workers at work"). For the calculation, you must use the maximum pressure expected (worst-case). If the value exceeds 50 [bar * L], a consultation with the Orga-Team is strictly recommended.



2. Temperature

- Temperature units:
 - Use consistent temperature units choose between absolute temperature [K] or relative temperature [°C]
- Maximum Temperature:
 - What is the maximum temperature expected during normal operation of the ChemCar?
 <u>All</u> calculations and their basis must be documented.
 Please discuss why the temperature you described is the maximum temperature during normal operation.
- Thermal hazard potential:
 - Are flash points or ignition points of one or more substances reached?
 - Is there any risk that thermal decomposition of one or more substances occurs? What decomposition products are formed?
 - What secondary reactions can take place?
 - How big is the resulting temperature in this case?
 - Other consequences, etc.?
- Adiabatic temperature increase / decrease:
 - Is the reaction exothermic or endothermic?
 - What reaction kinetics does the reaction have?
 - What temperature increase or decrease occurs under adiabatic conditions?

The complete reaction of maximum quantities of the reactants must be considered.

<u>Note</u>: The calculation of adiabatic temperature change is always possible. Experiments will be taken as an additional source of information only.

- Results of temperature increase or decrease must be discussed in the safety concept.
- Hot surfaces:
 - What temperatures can be generated at accessible surfaces?
 - Is it possible that burns due to hot surfaces can occur (guideline: T > 60 °C)?
 - Is protection against contact necessary?

- Cold surfaces:
 - How cold can accessible surfaces get (by reactions or filling processes)?
 - Is it possible to get injuries due to cold surfaces, e. g. frostbites or cold burns (guideline: T < 0 °C)?
 - Is protection against contact necessary?



3. Emissions

- Exhaust emission:
 - Are exhaust gases released before, during or after operation?
 Which exhaust gases are released (e. g. CO₂, O₂...)?
 - Which quantities are released in maximum (please document calculations)?
 - What is the maximal released substance concentration in the surrounding area? Please make comprehensible assumptions for calculating the substance concentration!
 - What are the limits (critical values) for the released substance (→ toxicity...)?
 Please write down the important limits (critical values) and discuss them.
 - Is the existing ventilation sufficient to minimize or prevent the danger from released substances?

<u>If n e c e s s a r y</u>: Please describe retention concept for all gases that must not be released into the surrounding.

<u>Note:</u>

According to the rules of ChemCar competition **release of minor amounts of hydrogen** resulting from a side reaction (especially parasitic reaction within an electro chemic battery) are allowed. However, this minor amount must be calculated, and safety issues must be assessed while creating the safety concept. If the data concerning the formation of hydrogen is incomplete use comprehensible assumptions which must be presented in detail in the safety concept.

- Noise emission:
 - What is the maximum noise level expected during operation?
 - Is it possible that injuries / impairments occur due to noise exposure (performer and viewers)?



4. Procedure

- Filling / dosing:
 - How is the reactor filled?
 - How are the educts dosed?
 - Is a wrong filling or wrong dosing possible?
 - What consequences can a wrong filling / dosing have?
- Leakage / unintended release:

This refers to a leakage during operation – competition in the hall.

- What dangers could be caused by leakage or accidental release?
- What measures should be taken in case of a leak or an unintentional release (especially liquid leakages)?
- Is there a retention concept, e. g. collecting basins?
- What kind of personal protective equipment is necessary in case of unintended release? Note:

The handling of unintended release or leakage during work at the ChemCar in preparation room must be described also.

- Mechanical function:
 - How is the force transmitted?
 - What happens during a mechanical blockage? For example, the blocking of wheels? Is it possible that a hazardous situation can develop?
- Intended mode of operation
 - How is the intended mode of operation defined?
 - How is it planned that the ChemCar after executing the starting action before the run will be provided with energy, starts to move, moves on (running) and finally stops?
 - How is the material flow during intended mode of operation?
- Emergency Shutdown
 - Is there an emergency shutdown mechanism?
 - How does this mechanism work? Description of manual function.

- Transport to starting line
 - Do you use one or more transport locks that have to be removed before the ChemCar is put on the starting line and started with the single-action? Are there eventually other precautions to take, when the ChemCar is transported to the starting line?



5. Documentation

- Basic documents:
 - A detailed functional description of the ChemCar
 - A photo or drawing of ChemCar (even unfinished ChemCar as status quo please add date of picture and state of assembly of ChemCar OR show separate part / steps of construction)
 Please label the parts of the ChemCar – counts for drawings and photos
 - A block flow diagram of the process
 - P&ID of the ChemCar. Pay attention to completeness (piping, inscriptions etc.). Please keep in mind the difference to a block flow diagram
 - Safety Data Sheets of all existing substances (both used substances and produced) please keep in mind that SDS must be up to date (ideally not older than 2 years!)
 - H- and P-phrases in written form (not only abbreviations)
 - Summary of all used substances with quantities in a register of hazardous substances
- Operating principle:
 - Description of the relevant system components (turbine, safety-bags etc.) and how they work
- Operating instructions:
 - Operating instructions according to TRGS 555 and GefStoffV § 14 for used reactants, products and potential auxiliaries. In the operating instructions the risks (explosive, oxidizing, toxic etc.), preventable conditions, transport, handling and disposal of the substance must be explained briefly. The minimum required personal protective equipment should be apparent from the operating instructions. An example of an operation instruction is shown in chapter 9.

► A Safety Data Sheet is no operation instruction but can be used as source of information in preparation of an operation instruction (see. Appendix to TRGS 555)!!!

<u>Note:</u> A separate operating instructions is needed for each substance. An operating instruction for the ChemCar is optional only.

- Reaction Equation:
 - Document the complete (!) reaction equation, including all side reactions and intermediates

- Calculations:
 - All calculation methods must be documented (maximum temperature, maximum pressure, temperature increase etc.). Not only the results.
 If an Excel-Sheet is used please pay attention to confirmability of the documentation!
- Suitability of the material:
 - Are used materials suitable?
 - Is corrosion or embrittlement of material possible, caused by used or formed substances?
 - Are the used materials suitable for the existing temperature ranges?

<u>Note:</u>

All components of the ChemCar must be considered in this context. For all components that may come into contact with substances / chemicals (educts, intermediate products, products) a material suitability must be proved. This means that it must be clarified if the utilised materials could interact with the substances / chemicals under operating conditions. Especially damages or malfunctions of the ChemCar must be taken into consideration, i. e. is a retention of released substances ensured? Is it possible that released substances interact with the retention equipment and affect the retention function significantly?

The proof of the material compatibility (manufacturer specifications, laboratory tests etc.) especially with the chemicals (\rightarrow educts, products AND intermediate products) is an essential part of the safety concept.

If you hand in lists of material suitability, the meant suitability should be highlighted clearly. It is not necessary to hand in a complete list. The front page and the page with the marked passage are sufficient.



6. Risk assessment

The purpose of a risk assessment is the coverage of the intended use and any faults. The consequences of a disturbance must be referred to the specific application. A reference to the Safety Data Sheet (general application) is not enough!

In addition to resulting hazards (e. g. explosion risk) caused from the used substances those caused by material properties (glass containers ► splinter protection) or components (fast rotating components ► cover) should be considered also.

Example for a risk assessment (Safety-Analysis Form):

Sequence of Steps	Potential Hazards	Procedure to Control Hazard	PPE or Equipment Required
Emergency shut- down			
	Hazard A (z. B. pressure increase)	Procedure A (z. B. stop educts supply, Opening of the safety valve)	PPE A, B, C (z. B. safety glasses, gloves and gowns)
Start-Up Procedure			
Run Time Procedure			
Shutdown Procedure			
Cleanup / Waste			
Dispusai			

Example for a hazardous substances register:

Chemical Information Page

Fill in as much data below as available. **Be sure to list the units!** If data are not available, leave the field blank. Material safety Datasheet (MSDS/SDS) for each named hazardous material is mandatory.

Chemical Quantities: List below the chemical names, concentrations, and total quantity of chemical required for the competition.

Chemical Name	Chemical State Solid, Liquid, Gas	Concentration Required	Total Quantity Required for Competition	Specific Personal Protective Equipment / Remarks

Chemical Properties and Hazards for ALL CHEMICALS, including reactants, solvents. intermediates and products.

Chemical Name	Physical State	GHS Symbol(s)	H&P- Statements (No. only)		Incompatible Chemicals List chemicals present within the	Flash Point Temp.
	S, L, G		Hazard Statements	Precautionary Statements	laboratory, and any others that may come in contact.	



7. Example: Calculation of the thermal hazard potential



To calculate the power, which is needed to absolve the required distance in addition of a given weight, this calculation chart is used. The ideal gas law is used to charge the required amount of released gas (here: CO_2) to run a piston engine. The application quantity is given by the stoichiometry of the reaction. The correction is made by experimental data. The heat capacity and the density is assumed as the value of water, because all educts are in liquid form or dissolved in this phase.



8. Example for the design of a safety valve

Resource: AD2000-A2: SAFETY VALVE

01	Opening Pressure		1 bar _g				
02	Item Number		d ₀ = 18 mm,				
02	$\alpha = 0.54$						
03	Reference	Reference					
04	Resource	11	A D2000-A2	Malaa	Demende		
05		Unit	Formula / Symbol	Value	Remark		
00	Surroundings Data	_	2				
07	External Pressure	Pa	Ps	1,01E+05			
08	Internal Pressure	Pa	P ₀	2,01E+05	1 barg		
09	Tempreture	К	Т	293,15			
10	Passage Surface	m ²	A ₀	0,0003	d = 18 mm		
11	Effluent Number	-	α	0,54			
12	Thermodynamic Data						
13	Substance Notation			28,2 Vol.% NH₃	mixture		
14	Molar Mass	kg/mol	М	not necessary			
15	Compressibility	-	Ζ	0,889			
16	Isentropic Exponent	-	κ	1,4			
17	Results						
18	Maximal Mass Flow	kg/s	$\dot{m} = \alpha \cdot A_0 \cdot \eta \cdot \sqrt{2 \alpha P_0}$	2,26E-01			
19	Maximal Mass Flow	kg/h	$m = \alpha n_0 \phi \sqrt{2p_g r_0}$	8126,1807			
20	Maximal Volume Flow	Nm ³ /s	$\dot{V}_N = -\frac{\dot{m}}{2}$	1,38E-01	Standard Volume		
21	Maximal Volume Flow	Nm³/h	ρ_{gN}	497,014			
22	Flow Profile	-		critical			
23	Calculation Part						
24	Gas Density	kg/m³	$ ho_g = rac{P \cdot M}{R \cdot Z \cdot T}$	28,531			
25	Standard Gas Density	kg/m³	$\rho_{gN} = \frac{101300[Pa] \cdot M}{R \cdot 273, 15[K]}$	1,635			
26	Pressure Relation In/External	-	$\eta_0 = \frac{P_S}{P_0}$	0,503			
27	Critical Pressure Relation	-	$\eta_{crit} = \left(\frac{2}{\kappa+1}\right)^{\frac{\kappa}{\kappa-1}}$	0,528			
28	Pressure Relation	-	$\eta = \begin{cases} \eta_{crit} > \eta_0 -> \eta_{crit} \\ \eta_{crit} \le \eta_0 -> \eta_0 \end{cases}$	0,528			
29	Effluent Function	-	$\psi = \sqrt{\left(\frac{\kappa}{\kappa-1} \cdot \left(\eta^{\frac{2}{\kappa}} \cdot \left(1 - \eta^{\frac{\kappa-1}{\kappa}}\right)\right)\right)}$	0,484			



9. Example: instruction manual according to TRGS 555/GefStoffV § 14





10. References

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2.	https://gestis.dguv.de/	GESTIS-Stoffdatenbank: Gefahrstoffinformationssystem der Deutschen
		Gesetzlichen Unfallversicherung
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4.	http://www.baua.de/de/Themen-	TRGS 555 "Betriebsanweisung und Information der
	von-A-Z/Gefahrstoffe/TRGS/TRGS-	Beschäftigten" (PDF-Datei, 98 KB)
	<u>555.html</u>	
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